

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
13 December 2001 (13.12.2001)

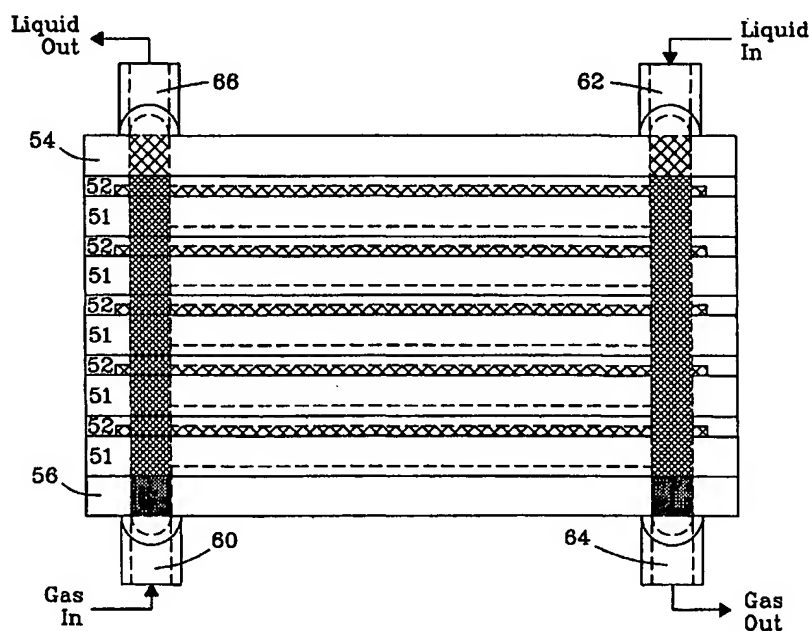
PCT

(10) International Publication Number
WO 01/93976 A2

- (51) International Patent Classification⁷: **B01D 17/00**
- (21) International Application Number: **PCT/US01/17622**
- (22) International Filing Date: **30 May 2001 (30.05.2001)**
- (25) Filing Language: **English**
- (26) Publication Language: **English**
- (30) Priority Data:
09/588.871 6 June 2000 (06.06.2000) **US**
- (71) Applicant: **BATTELLE MEMORIAL INSTITUTE**
[US/US]; Pacific Northwest Division, Intellectual Property Services, P.O. Box 999, Richland, WA 99352 (US).
- (72) Inventors: **TEGROTENHUIS, Ward, E.**; 8813 West Grande Rhonde, Kennewick, WA 99336 (US). **WEGENG, Robert, S.**; 2603 Harris Avenue, Richland, WA 99352 (US). **WHYATT, Greg, A.**; 3401 Equestrian Drive, West Richland, WA 99353 (US). **STENKAMP, Victoria, S.**; 315 Spokane Street, Richland, WA 99352 (US). **GAUGLITZ, Phillip, A.**; 183 Newhaven Place, Richland, WA 99352 (US).
- (74) Agent: **MAY, Stephen, R.**; Battelle Memorial Institute, Pacific Northwest Division, Intellectual Property Services, P.O. Box 999, MSIN: K1-53, Richland, WA 99352 (US).
- (81) Designated States (*national*): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, UZ, VN, YU, ZA, ZW.
- (84) Designated States (*regional*): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).
- Published:
— *without international search report and to be republished upon receipt of that report*

[Continued on next page]

(54) Title: **MICROSYSTEM CAPILLARY SEPARATIONS**



(57) Abstract: Laminated, multiphase separators and contactors having wicking structures and gas flow channels are described. Some preferred embodiments are combined with microchannel heat exchange. Integrated systems containing these components are also part of the present invention.

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For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

MICROSYSTEM CAPILLARY SEPARATIONS

FIELD OF THE INVENTION

5 The present invention relates to processes and devices that utilize capillary forces to separate fluids. Several of the inventive embodiments are limited to microcomponent or microchannel devices that utilize capillary forces.

BACKGROUND OF THE INVENTION

10 Compact systems for capturing and/or separating fluids are desirable in a variety of applications. For example, hydrogen-powered vehicles could utilize fuel cells that recycle water. As another example, efficient and lightweight systems for recovery and reuse of water in spacecraft has long been recognized as a requirement for human space exploration. The present invention provides
15 methods and apparatus for efficient fluid capture and separation.

SUMMARY OF THE INVENTION

 The invention provides methods and apparatus for separating fluids and/or heat exchange. One process separates fluids by passing a mixture of at
20 least two fluids, comprising a first fluid and a second fluid, into a device having at least one channel. The channel has an open area and a wicking region. The first fluid is either a liquid (such as a droplet or liquid particle) that is sorbed by the wicking region, or a gas that, under separation conditions, forms a liquid in the wicking region. The first liquid travels through the wicking region to a liquid
25 flow channel and then exits the device through a liquid exit channel. The second fluid is a gas that passes through the gas flow channel to a gas exit, and exits the device through the gas exit.

 The invention also provides a process of contacting fluids in which at least two fluids are passed into a device having at least one channel. The channel
30 has an open area and a wicking region and an interface between the wicking region and the open area. During operation, at least one fluid flows through the wicking region, and at least one other fluid flows through the open area. At the

interface between the wicking region and the open area, one fluid contacts at least one other immiscible fluid, and there is mass transfer occurring through the interface between the at least one fluid flowing through the wicking region, and the at least one other fluid flowing through the open area.

5 The invention further provides a method of condensing a liquid in which a gas passes into a device having at least one channel. The channel has an open area and a wicking region and is in thermal contact with at least one microchannel heat exchanger; and a heat exchange fluid is passed through the microchannel heat exchanger(s). During operation heat is removed from the gas
10 stream causing some part to condense to form a liquid. Said formed liquid is sorbed into the wicking region, travels through the wicking region to a liquid flow channel and then exits the device through a liquid exit channel.

 The invention further provides an apparatus having at least one channel comprising an open area and a wick. The wick in the channel is connected to an
15 exit wick, and the open area is connected to a gas exit. This apparatus is useful for many of the processes described herein.

 The invention also provides a liquid condenser comprising at least one channel; wherein the channel comprises a gas flow channel and a wick. The channel is in thermal contact with at least one microchannel heat exchanger.
20 Both the apparatus and condenser are particularly well suited for use in a chemical reactor.

 The presence of wicks and optional pore throats and capture structures are common to multiple embodiments of the invention. A wick is a material that will preferentially retain a wetting fluid by capillary forces and through which there
25 are multiple continuous channels through which liquids may travel by capillary flow. The channels can be regularly or irregularly shaped. Liquid will migrate through a dry wick, while liquid in a liquid-containing wick can be transported by applying a pressure differential, such as suction, to a part or parts of the wick. The capillary pore size in the wick can be selected based on the contact angle of
30 the liquid and the intended pressure gradient in the device, and the surface tension of the liquid. Preferably, the pressure at which gas will intrude into the

wick should be greater than the pressure differential across the wick during operation - this will exclude gas from the wick.

The liquid preferentially resides in the wick due to surface forces, i.e. wettability, and is held there by interfacial tension. The liquid prefers the wick to the gas channel and as long as there is capacity in the wick, liquid is removed from the gas stream and does not leave in the gas stream.

The wick can be made of different materials depending on the liquid that is intended to be transported through the wick. The wick could be a uniform material, a mixture of materials, a composite material, or a gradient material. For example, the wick could be graded by pore size or wettability to help drain liquid in a desired direction. Examples of wick materials suitable for use in the invention include: sintered metals, metal screens, metal foams, polymer fibers including cellulosic fibers, or other wetting, porous materials. The capillary pore sizes in the wick materials are preferably in the range of 10 nm to 1 mm, more preferably 100 nm to 0.1 mm, where these sizes are the largest pore diameters in the cross-section of a wick observed by scanning electron microscopy (SEM). In a preferred embodiment, the wick is, or includes, a microchannel structure. Liquid in the microchannels migrates by capillary flow. The microchannels can be of any length, preferably the microchannels have a depth of 1 to 1000 micrometers (μm), more preferably 10 to 500 μm . Preferably the microchannels have a width of 1 to 1000 μm , more preferably 10 to 100 μm . In a preferred embodiment, the microchannels are microgrooves, that is, having a constant or decreasing width from the top to the bottom of the groove. In another embodiment, the microchannels form the mouth to a larger diameter pore for liquid transport.

The wick is preferably not permitted to dry out during operation since this could result in gas escaping through the wick. One approach for avoiding dryout is to add a flow restrictor in capillary contact with the wick structure, such as a porous structure with a smaller pore size than the wick structure and limiting the magnitude of the suction pressure such that the non-wetting phase(s) cannot displace the wetting phase from the flow restrictor. This type of restrictor is also known as a pore throat. In preferred embodiments, a pore throat is provided

between the wick and the liquid flow channel and/or at the liquid outlet. In some embodiments, the wick can have a small pore diameter such that it serves to transport fluids from the gas channel and also prevents gas intrusion, thus serving the dual purpose of a wick and a pore throat.

5 A pore throat has a bubble point that is greater than the maximum pressure difference across the pore throat during operation. This precludes intrusion of gas into the pore throat due to capillary forces (surface tension, wettability, and contact angle dependent). The pore throat should seal the liquid exit, so there should be a seal around the pore throat or the pore throat should
10 cover the exit in order to prevent gas from bypassing the pore throat. The pore throat is preferably very thin to maximize liquid flow through the pore throat at a give pressure drop across the pore throat. Preferably, the pore throat has a pore size that is less than half that of the wick and a thickness of 50% or less than the wick's thickness; more preferably the pore throat has a pore size that is 20% or
15 less that of the wick. Preferably, the pore throat is in capillary contact with the wicking material to prevent gas from being trapped between the wick and the pore throat and blocking the exit.

 Flooding can result from exceeding the flow capacity of the device for wetting phase through the wick; the flow capacity is determined by the pore
20 structure of the wick, the cross-sectional area for flow, or the pressure drop in the wick in the direction of flow.

 A capture structure can be inserted (at least partly) within the gas flow channel, and in liquid contact with the wick. The capture structure assists in removing (capturing) a liquid from the gas stream. One example of a capture
25 structure are cones that protrude from the wick; liquid can condense on the cones and migrate into the wick - an example of this capture structure is shown in U.S. Patent No. 3,289,752, incorporated herein by reference. Other capture structures include inverted cones, a liquid-nonwetting porous structure having a pore size gradient with pore sizes getting larger toward the wick, a liquid-wetting
30 porous structure having a pore size gradient with pore sizes getting smaller toward the wick and fibers such as found in commercial demisters or filter media. Mechanisms for capturing dispersed liquid particles include impingement (due to

flow around obstructions), Brownian capture (long residence time in high surface area structure), gravity, centrifugal forces (high curvature in flow), or incorporating fields, such as electrical or sonic fields, to induce aerosol particle motion relative to the flow field.

5 Nonwetting surfaces can be disposed on the gas flow channel walls. These nonwetting surfaces can help prevent formation of a liquid film on the surface and, in combination with a wick or a wick and capture structure the liquid present in a fluid mixture can be siphoned away from the condensing surface by capillary flow, thereby avoiding problems associated with dropwise
10 condensation, such as cold spots or re-entrainment.

 The invention, in various aspects and embodiments can provide numerous advantages including: rapid mass transport, high rates of heat transfer, low cost, durability, and highly efficient liquid separations in a compact space.

15 Devices and processes of the present invention are capable of integrating high efficiency, high power density heat exchange. Heat exchange can facilitate phase changes within the separation device, such as condensation and evaporation. One example is partial condensation of a gas stream to recover condensable components, such as water from the cathode waste gas stream
20 from a fuel cell. Another optional feature is reduced or non-wettability of the wall adjacent to a heat exchange surface to preclude formation of a liquid film. The heat transfer coefficient would increase substantially by avoiding the resistance of a liquid film.

 The embodiments show preferred embodiments in which there are
25 multiple gas flow channels operating in parallel. This configuration allows high throughput and provides a large surface area to volume ratio for high efficiency. In some preferred embodiments, layers are stacked to have between 2 and 600 separate gas flow channels, more preferably between 4 and 40 gas flow channels. As an alternative to the parallel arrangement, the channels could be
30 connected in series to create a longer flow path.

 Another advantageous feature of some preferred embodiments of the invention is that the gas flow channels and/or liquid flow channels are essentially

planar in the fluid separation regions. This configuration enables highly rapid and uniform rates of mass and heat transport. In some preferred embodiments, the gas flow channels and/or liquid flow channels have dimensions of width and length that are at least 10 times larger than the dimension of height (which is perpendicular to net gas flow).

The subject matter of the present invention is distinctly claimed in the concluding portion of this specification. However, both the organization and method of operation, together with further advantages and objects thereof, may further be understood by reference to the following description taken in connection with accompanying drawings wherein like reference characters refer to like elements.

GLOSSARY OF TERMS

15

A "capture structure" is a structure disposed (at least partly) within a gas flow channel that assists movement of a liquid into the wick.

A "cell" refers to a separate component, or an area within an integrated device, in which at least one unit operation is performed. In preferred embodiments, the cell has a width less than about 20 cm, length less than about 20 cm, and height less than about 3 cm.

"Device volume" refers to the entire volume of the device, including channels, headers, and shims.

"Entrainment" refers to transport of liquid into the gas exit

"Flow microchannel" refers to a microchannel through which a fluid flows during normal operation of an apparatus.

A "laminated device" is a device having at least two nonidentical layers, wherein these at least two nonidentical layers can perform a unit operation, such as heat transfer, condensation, etc., and where each of the two nonidentical layers are capable having a fluid flow through the layer. In the present invention, a laminated device is not a bundle of fibers in a fluid medium.

A "liquid" is a substance that is in the liquid phase within the wick under the relevant operating conditions.

"Microchannel" refers to a channel having at least one dimension of 5 mm or less. The length of a microchannel is defined as the furthest direction a fluid could flow, during normal operation, before hitting a wall. The width and depth are perpendicular to length, and to each other, and, in the illustrated embodiments, width is measured in the plane of a shim or layer.

"Microcomponent" is a component that, during operation, is part of a unit process operation and has a dimension that is 1 mm or less.

10 "Microcomponent cell" is a cell within a device wherein the cell contains microcomponents.

"Pore throat" refers to a porous structure having a maximum pore dimension such that a non-wetting fluid is restricted from displacing a wetting fluid contained with the pore throat under normal operating conditions.

15 "Residence time" refers to the time that a fluid occupies a given working volume.

"Unit process operation" refers to an operation in which the chemical or physical properties of a fluid stream are modified. Unit process operations (also called unit operations) may include modifications in a fluid stream's temperature, pressure or composition.

20 A "wicking region" is the volume occupied by a wick, or, a wicking surface such as a grooved microchannel surface.

"Working volume" refers to the total channel volume of the device, and excludes the headers and solid shim and end plate materials.

25

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a cross-sectional view of a gas/liquid separator.

30

FIG. 2 is a top-down view of a gas flow channel layer of the gas/liquid separator.

FIG. 3 is a bottom-up view of a liquid flow channel layer of the gas/liquid separator.

5 FIG. 4 is a top-down view of an end plate of the gas/liquid separator.

FIG. 5 illustrates the other end plate of the gas/liquid separator.

10 FIG. 6 is a cross-sectional view of a gas/liquid contactor.

FIG. 7 is a top-down view of a gas flow channel layer of the gas/liquid contactor.

15 FIG. 8 is a bottom-up view of a liquid flow channel layer of the gas/liquid contactor.

FIG. 9 illustrates a wick insert.

20 FIG. 10 is a cross-sectional view of a counter-current heat exchange condensor assembly.

FIG. 11 is a top-down view of a gas flow channel layer of the counter-current heat exchange condensor assembly.

25 FIG. 12 is a bottom-up view of a liquid flow channel layer of the counter-current heat exchange condensor assembly.

FIG. 13 is a top-down view of a heat exchange layer of the counter-current heat exchange condensor assembly.

30 FIG. 14 is a cross-sectional view of a cross-current heat exchange condensor assembly.

FIG. 15 is a top-down view of a gas flow channel layer of the cross-current heat exchange condensor assembly.

5 FIG. 16 is a bottom-up view of a liquid flow channel layer of the cross-current heat exchange condensor assembly.

FIG. 17 is a top-down view of a heat exchange layer of the cross-current heat exchange condensor assembly.

10

FIG. 18 is a data plot from the Examples showing maximum water flow rate with no entrainment as a function of gas flow rate.

DETAILED DESCRIPTION

15 In a first aspect, the invention provides a gas/liquid separator. An embodiment of on such device is illustrated in **Fig. 1**. The illustrated device is made up of end plates **6, 8** and alternating central shims **1** and **2**. A fluid inlet **9** is connected to open channel **12**. Shim **1** has open gas flow channels **14**. The surface **18** of solid section **16** forms the bottom of the gas flow channel. The top
20 of the gas flow channel is formed wick **22** of shim **2**. As the gas/liquid mixture flows through channel **14**, the liquid component is absorbed by the wick **22**. The liquid in the wick travels to a wick exit channel and flows out through liquid outlet **29**. To remove liquid suction can be applied through a pump (not shown). Gas flows out through a separate channel and out through gas outlet **19**.

25 A top down view of shim **1** is illustrated in **Fig. 2**. Channels **14** are separated by lands **32**. The lands can support a wick insert and prevent channel collapse during fabrication. Gas flows through channels **14** and into gas exit holes **34**. Lands **32** are preferably the same height as edges **36**. The height of the gas flow channels **14**, from surface **18** to wick surface **24** is preferably about
30 10 μ m to 5 mm, more preferably 100 μ m to 1 mm. The height of the channels is preferably small for good heat and mass transfer and overall device size, balanced against potentially slower flow rates. The path to exit wicks **42** can be

blocked by lands 38. A high ratio of surface area of exposed wick to volume of gas flow channel is desirable for efficient phase separations. Preferably this ratio is from 1 to 1000 cm²:cm³, more preferably from 5 to 100.

A bottom up view of shim 2 (without wick) is illustrated in Fig. 3. It includes gas exit holes 34 (open space) and exit wicks 42. A wick (not shown) may be inserted open space 42 (preferably without blocking hole 12). Alternatively, surface of the shim can be a wick structure such as microchannels. In any event, the wick structure should create a continuous liquid flow path with exit wick 42, but should not block gas exit holes 34.

Fig. 4 illustrates a top down view of end plate 6 showing spaces for gas/liquid entry 12 and gas exit holes 34. Fig. 5 illustrates end plate 8 with exit wicks 42. Of course, the device could be plumbed to have gas and liquid exit from the same side or the gas/liq entry could be moved to the opposite end plate 8 to have liquid exit and gas/liq entry on the same side of the device.

In operation of a device with a wick, the wick should not be flooded, and it is preferably not dry. A wet or saturated wick will effectively transport liquid through capillary to a low pressure zone, such as low pressure created by suction. A pore throat may be added to liquid outlet 27 to prevent gas flow out of liquid exit.

A cross-sectional view of a gas/liquid contactor is illustrated in Fig. 6. This contactor has end plates 54 and 56 and alternating shims 51 and 52. T-joint inlets 60 and 62 are for the passage of gas and liquid respectively. T-joint outlets 64 and 66 are for the passage of gas and liquid respectively. A top-down view of shim 51 is illustrated in Fig. 7. Gas flows in through gas inlet holes 76 and out through outlet holes 72. A bottom-up view of shim 52 is illustrated in Fig. 8. Liquid flows in through wick channels 82 through the wick and out through wick channels 84. A wick insert is illustrated in Fig. 9. The wick insert has through holes 92 for gas flow through the wick. Regions 94 of the insert can be continuous wick or can be holes that are filled with a continuous wick through the wick channels. Where the wick insert covers regions 94, disks or other inserts of a wicking material should be disposed in channels 78, 79, 82 and 84 to provide a continuous capillary liquid flow path. Use of microchannels in shim 52

can obviate the need for a wick insert. Endplate 54 has wick channels (not shown) corresponding to the wick channels in shim 52. Endplate 56 has gas inlet and outlet holes (not shown) corresponding to inlet and outlet holes 72 and 76. This device illustrates a preferred counterflow of liquid and gas phases.

- 5 Where the liquid is used to selectively absorb components from the gas phase, the counterflow construction contacts the gas with the lowest concentration of extractable components with the purest liquid and thus provides for maximal absorption of the gas components.

A cross-sectional view of a counter flow heat exchange condenser assembly 100 is illustrated in Fig. 10. The assembly includes shims 101, 102, 103, inlets 104 and 105, and outlets 106, 108, and 110. Shim 102 includes wick 112 and wall 124. Shim 101 has gas flow channels 114 and walls 126. Heat exchanger shim 103 contains microchannels 166 and wall 122.

A top down view of shim 101 is illustrated in Fig. 11. The illustrated shim 15 contains gas flow channels 118, fluid flow inlets 113, lands 116, gas exit holes 117, heat exchange fluid holes 115, and liquid exit hole 119.

Fig. 12 illustrates a bottom up view of shim 102. The illustrated shim includes liquid flow channel 128, fluid flow inlets 123, gas exit holes 127, heat exchange fluid holes 125, and liquid exit hole 129.

20 A top down view of a heat exchange shim is illustrated in Fig. 13. The heat exchange fluid enters through holes 132, travels through microchannels 134 and exits through holes 136. Passageways 137, 138, and 139 are provided for fluid mixture, gas and liquid to flow through the heat exchange shim.

Endplate 190 has inlet and outlet holes for the heat exchange fluids. Endplate 111 has fluid inlet holes, gas outlet holes, and liquid exit holes.

25 During operation, a fluid mixture can enter through inlet 105 and pass through gas flow channels 114. A heat exchange fluid enters through inlet 104 and passes through microchannel layer 116. In a preferred embodiment, one component of the fluid mixture mixture condenses in wick 112. Heat can be removed from (or added to) the system by the heat exchange fluid. Depending on system requirements, either wall 101 or walls 122, 124 can be insulating. In a preferred embodiment, the layers (shims) are arranged to have the repeating

sequence: wick, gas flow channel, wall, microchannel layer, wall, gas flow channel, and wick.

A cross-current heat exchange assembly is illustrated in Figs. 14-17. The gas and liquid inlets and outlets and the lands are indicated using the same
5 shadings as above. In this embodiment, the heat exchange fluid runs cross-current (at a right angle) to the flow of fluid through the gas flow channel.

The figures illustrate preferred embodiments in which liquid flows by direct contact of the wick in the liquid flow channels to a wick in the liquid exit channels. In other embodiments, however, the liquid, after having been sorbed into the
10 wick, can flow into a liquid flow channel that does not contain a wick. The liquid can then flow out through wicks or by fluid flow without wicks.

The shims can be made of metals, plastics, ceramic or composite materials. Metal shims can be made by etching, conventional cutting and machining, electrical discharge machining (EDM), laser machining, stamping, or
15 molding techniques. Plastic shims can be made using the same techniques or by conventional plastic forming techniques, including injection molding, hot embossing, stamping, casting, and other molding techniques. Ceramic shims could be made using techniques well known for fabricating ceramic parts, including those used in fabricating solid oxide fuel cell elements. The shim
20 material facing the gas channel can be made hydrophobic through coatings, treatment or by the choice of material. The end plates are preferably made of a similar material as the shims and made using similar techniques. The shims are stacked with wicks installed within the liquid flow channel, either held in loosely
25 by the lands and channel walls or by adhering the wicks to the liquid channel wall. The wick or pore throat must prevent an open path for the gas to flow to the liquid exit. This is accomplished either by close tolerances between the wick or pore throat structure and the walls, by using a sealant, such as epoxy to install the wick or pore throat, or through the use of gaskets or o-rings. End plates are then placed on the top and bottom of the shim stack. The seams between shims
30 and between end plates and shims are either sealed by bonding or by a compression seal. Bonding can be accomplished by diffusion bonding, by chemical reaction, such as using an epoxy resin, or by gluing with an adhesive

material. A compression seal can be accomplished using gaskets, O-rings, or by surface to surface contact and bolting the device together. Inlets and outlets can be connected by the same methods, by welding, by screws or bolts, or by other known connection techniques.

5 When making low volumes of a given device or when the device needs to be disassembled for cleaning or modifications, the preferred fabrication technique is to fabricate the shims and end plates by conventional machining, such as by milling. Seals between the shims and end plates are preferably accomplished by compression seals using either O-rings placed in grooves
10 machined into one of the sealing surfaces or by using a gasket material cut to match the profile of the sealing surface. The device is then held together in compression using bolts. The liquid exit is isolated from the gas flow channel using gaskets or sealant, such as epoxy, between the wick or pore throat and the wall. Inlets and outlets can be installed using standard threaded fittings or other
15 known connection techniques.

 The devices and processes described herein are especially desirable for integration in a system. These systems can accomplish desired functions such as heat transfer, mass transfer, heterogeneous reaction, electrochemical reactions, or electric field enhancements. When integrated as an element in a
20 chemical reactor, the inventive devices can result in process intensification (e.g., reduced mass transport residence times) and/or greater than equilibrium conversion and selectivity for chemical reactions. Combination with a heat exchanger can facilitate multi-phase endothermic or exothermic chemical reactions.

25 Heterogeneous catalytic reactions can also be accomplished within the proposed architecture by impregnating active catalyst materials in the wicking structure for liquid phase reactions and/or in the capture structure for gas phase reaction. One example is Fischer-Tropsch synthesis, where condensable hydrocarbons are produced. Reactor residence time can be reduced by the
30 incorporation of structures that remove liquid hydrocarbon products in contact with the catalyst structure. The devices can also be used in an integral reactor-chemical separator. For example, the wick or an absorbent material within the

wick can selectively remove one of the products. This causes a shift in the equilibrium conversion as well as improved selectivity. Other, nonlimiting, examples include low temperature water gas shift reaction, where we believe that selectively removing CO could lower the operating temperature for achieving
5 adequate conversion. This effect could be enhanced by flowing an absorbent liquid countercurrent to a flowing gas stream.

Examples

Example 1:

10 Half inch polycarbonate was machined to create a 3000 μm deep x 2 cm wide x 8 cm long channel. An 1/8" NPT barbed fitting placed 1 cm from the end of the channel served as the liquid outlet. A 2 cm x 8 cm piece of 70x70 stainless steel mesh available from McMaster Carr was placed in the channel beneath a 1/16"x 2 cm x 8 cm piece of sintered nickel with 5 μm pores (Mott Corporation).
15 The sintered nickel was sealed into place using Loctite[®] RTV silicone adhesive.

A 0.25" piece of polycarbonate was machined so that two 1/8" NPT barbed fittings could be threaded into holes 6 cm apart. This piece of polycarbonate had been made hydrophobic by treatment in a capacitively coupled RF (13.56 MHz) plasma reactor (66x66x91cm³) using two stainless steel
20 parallel electrodes (25 cm in diam.). The electrodes were separated by a distance of 10 cm, and were both water-cooled. The RF power was applied to the upper electrode, and the sample was placed on the lower, grounded electrode. An automatic L-type matching network with two air variable capacitors converted the complex impedance of plasmas to 50 resistivity. A dc self-bias
25 meter with selectable scaling allowed precise control over the matching/chamber environment. The system was first evacuated to a base pressure of 10⁻⁵ Torr using a diffusion pump. The CF₄ gas was then introduced to the system and a pressure of 100 mTorr was established by adjusting the opening of a throttle valve placed between the diffusion pump and the chamber. After a stabilization
30 period of several minutes, the plasma was initiated. The treatment was performed at a power of 100W, a pressure of 100 mTorr, and a gas flow rate of 50 sccm for 5 minutes. (See "In-situ and real-time monitoring of plasma-

induced etching of PET and acrylic films", M. K. Shi, G.L. Graff, M.E. Gross, and P.M. Martin, Plasmas and Polymers, in press). The advancing contact angle of water on the plasma treated substrate was greater than 110° .

The half inch and quarter inch polycarbonate pieces were bolted together
5 and sealed with an o-ring such that the $3000\ \mu\text{m}$ channel and hydrophobic surface faced each other. The device volume was $90\ \text{cm}^3$. The device was situated so that the liquid outlet faced downwards. A 3" piece of $1/8"$ tubing was attached to the liquid outlet to provide suction by siphoning. The fitting in the $1/2"$ polycarbonate piece above the liquid outlet served as the gas outlet, while the
10 other fitting in the $1/2"$ polycarbonate served as the inlet to a mixture of air and water. Various flows of air were fed to the device. The water flow rate was adjusted to the maximum flow that allowed no entrainment of water in the gas exit line. This maximum flow is plotted as a function of gas flow rate (indicated as Mott in Figure 18). As can be seen, the maximum water flow rate was
15 constant at roughly 6.5 milliliters/min (mL/min) between the air flow rates of 500 and 1250 mL/min. Significant entrainment of the liquid occurred at 1500 mL/min air flow rate, until the liquid flow rate was decreased to 2.6 mL/min. No gas was observed to exit the liquid channel. Given that the working volume of the channels is $4.8\ \text{cm}^3$, the residence time is 0.2 seconds at the highest flow rate.

20

Example 2:

The device was the same as above, except a $1400\ \mu\text{m}$ channel replaced the $3000\ \mu\text{m}$ channel. This channel had a $8\ \text{cm} \times 2\ \text{cm}$ piece of 0.0011"
25 Supramesh from Pall Corporation placed in the bottom. This material consists of sintered stainless steel overlying a fine stainless mesh. Flat gasket material with a $1.5\ \text{cm} \times 7.5\ \text{cm}$ hole placed inside the channel served to seal both pieces of polycarbonate together as well as preventing gas intrusion into the porous material.

30 Again, the gas flow rate was plotted against the maximum liquid flow rate that allowed no entrainment of water in the gas exit line. These data are indicated as Pall in Figure 18. As can be seen, the water flow rate was close to

10 mL/min between the air flow rates of 200 and 1500 mL/min. At a gas flow rate of 1750 mL/min, entrainment occurred in the air exit until the liquid flow was decreased to 5 mL/min.

5 A comparison of the efficiency of this device with a typical centrifugal separator demonstrates the economy of size and weight of this invention. A known fuel processing stream contains 355 L/min of gas with 300 mL/min water. The size of a type T cast iron gas/liquid separator from Wright -Austin to treat this stream would be approximately 2100 cm³ and weigh 14 pounds. The residence time within the device is 0.35 seconds. In contrast, the invention
10 would have a working volume of approximately 450 cm³ giving a residence time of 0.08 seconds. The pressure drop across the Wright -Austin system is estimated to be 1.38 inches of water, while the pressure drop across the invention is estimated to be 0.075 inches of water.

15

CLOSURE

While preferred embodiments of the present invention have been shown and described, it will be apparent to those skilled in the art that many changes and modifications may be made without departing from the invention in its
20 broader aspects. The appended claims are therefore intended to cover all such changes and modifications as fall within the true spirit and scope of the invention.

CLAIMS

1. A process of separating fluids comprising:
5 passing a mixture of at least two fluids, comprising a first fluid and a second fluid, into a device having at least one channel; the channel comprising an open area and a wick, wherein the first fluid is sorbed by the wick;
 wherein the first fluid is a liquid in the wick that travels to a liquid exit; and
 wherein the first fluid exits the device through the liquid exit;
10 wherein the second fluid is a gas that passes through the open area to a gas exit, and wherein the gas exits the device through the gas exit.
2. The process of claim 1 wherein the liquid, without leaving a wick, travels through the wick to a wick in the liquid exit.
15
3. The process of claim 1 wherein the liquid pass through the wick to a liquid flow channel, and subsequently flows through the liquid flow channel to the liquid exit.
- 20 4. The process of claim 1 wherein the device further comprises a pore throat and the liquid flows through the pore throat prior to exiting the device.
5. The process of claim 4 wherein the pore throat is direct contact with the wick.
25
6. The process of claim 1 wherein a capture structure is disposed within the gas flow channel.
7. The process of claim 6 wherein the capture structure is a random
30 fiber mesh.

8. The process of claim 7 wherein the random fiber mesh has an asymmetric structure for inducing flow of liquid toward the wick.

9. The process of claim 6 wherein the capture structure is a regular
5 array of structures placed in the gas flow path and causing gas to flow around said structures.

10. The process of claim 9 wherein the regular array of structures has a shape that induces flow toward the wick.

10

11. The process of claim 6 wherein the capture structure causes the gas to flow in a curved path causing liquid to move toward a wall or the wick structure by centrifugal force.

12. The process of claim 1 wherein the open area is at least partly
15 defined by a wall that is nonwetting for said first fluid.

13. The process of claim 1 wherein the open area is a microchannel.

14. The process of claim 2 wherein said first fluid is water and said
20 second fluid is selected from the group consisting of carbon monoxide, carbon dioxide, methane and hydrogen.

15. A process of contacting fluids comprising:
25 passing at least two fluids into a device having at least one channel;
wherein the channel comprises an open area and a wick and an interface between the wick and the open area;
wherein the wick has a width, length and height that are mutually perpendicular, wherein the height is perpendicular to the interface, and wherein
30 the height of the wick is at least five times smaller than both the width and the length of the wick;

wherein at least one fluid flows through the wicking region, and at least one other fluid flows through the open area;

wherein, at the interface between the wick and the open area, one fluid contacts at least one other fluid; and further wherein there is mass transfer
5 occurring through the interface between the at least one fluid flowing through the wick, and the at least one other fluid flowing through the open area.

16. The process of claim 15 wherein the liquid travels through a wick until the liquid exits the device.

10

17. The process of claim 15 wherein the open area comprises a microchannel that is at least partly defined by a wall that is nonwetting for said first fluid.

15

18. The process of claim 15 wherein the open area comprises a microchannel and wherein fluid flow in the open area is in the direction opposite liquid flow in the wick.

20

19. The process of claim 18 wherein the device further comprises a microchannel heat exchanger that is in thermal contact with the open area.

25

20. A process of condensing a liquid comprising:
passing a gas into at least one channel of a device; wherein said at least one channel is in thermal contact with at least one microchannel heat
exchanger;

passing a heat exchange fluid through said at least one microchannel heat exchanger;

wherein heat is transferred between the at least one channel and the heat exchanger;

30

wherein at least a portion of said gas is condensed to a liquid within the channel;

the channel comprising an open area and a wick, wherein said condensed liquid is sorbed by the wick; and

wherein said condensed liquid in the wick travels to a liquid exit; and wherein the condensed liquid exits the device through the liquid exit.

5

21. The process of claim 20 wherein the heat transfer coefficient of the condensing fluid is less than the heat transfer coefficient of the heat exchange fluid.

10 22. The process of claim 20 comprising passing a gas into at least two channels of a device;

wherein each of the two channels comprise an open area and a wick;

wherein a microchannel heat exchanger is disposed between the two channels; and exchanging heat between the heat exchanger and each of the two
15 channels.

23. An apparatus having at least one channel; the channel comprising an open area and a wick; the wick in the channel is connected to an exit wick; wherein the open area is connected to a gas exit

20

24. A liquid condenser comprising: a laminated device comprising at least two channels; wherein each of said at least two channels comprise a gas flow channel and a wick; and wherein each of said at least two channels are in thermal contact with at least one microchannel heat exchanger.

25

25. A chemical reactor comprising the apparatus of claim 23.

26. A chemical reactor comprising the condenser of claim 24.

30 27. The process of claim 20 wherein the heat exchange fluid flows through said at least one microchannel heat exchanger in a direction perpendicular to the direction of flow of gas in said at least one channel.

28. The process of claim 20 wherein the heat exchange fluid flows through said at least one microchannel heat exchanger in a direction opposite to the direction of flow of gas in said at least one channel.

5

29. The process of claim 15 wherein a chemical reaction occurs in said at least one channel.

30. The process of claim 29 wherein said chemical reaction comprises a Fischer-Tropps synthesis reaction.

10

31. The process of claim 29 wherein said chemical reaction is a dehydrogenation reaction.

15

32. The process of claim 29 wherein said chemical reaction is a hydrocarbon reforming reaction.

20

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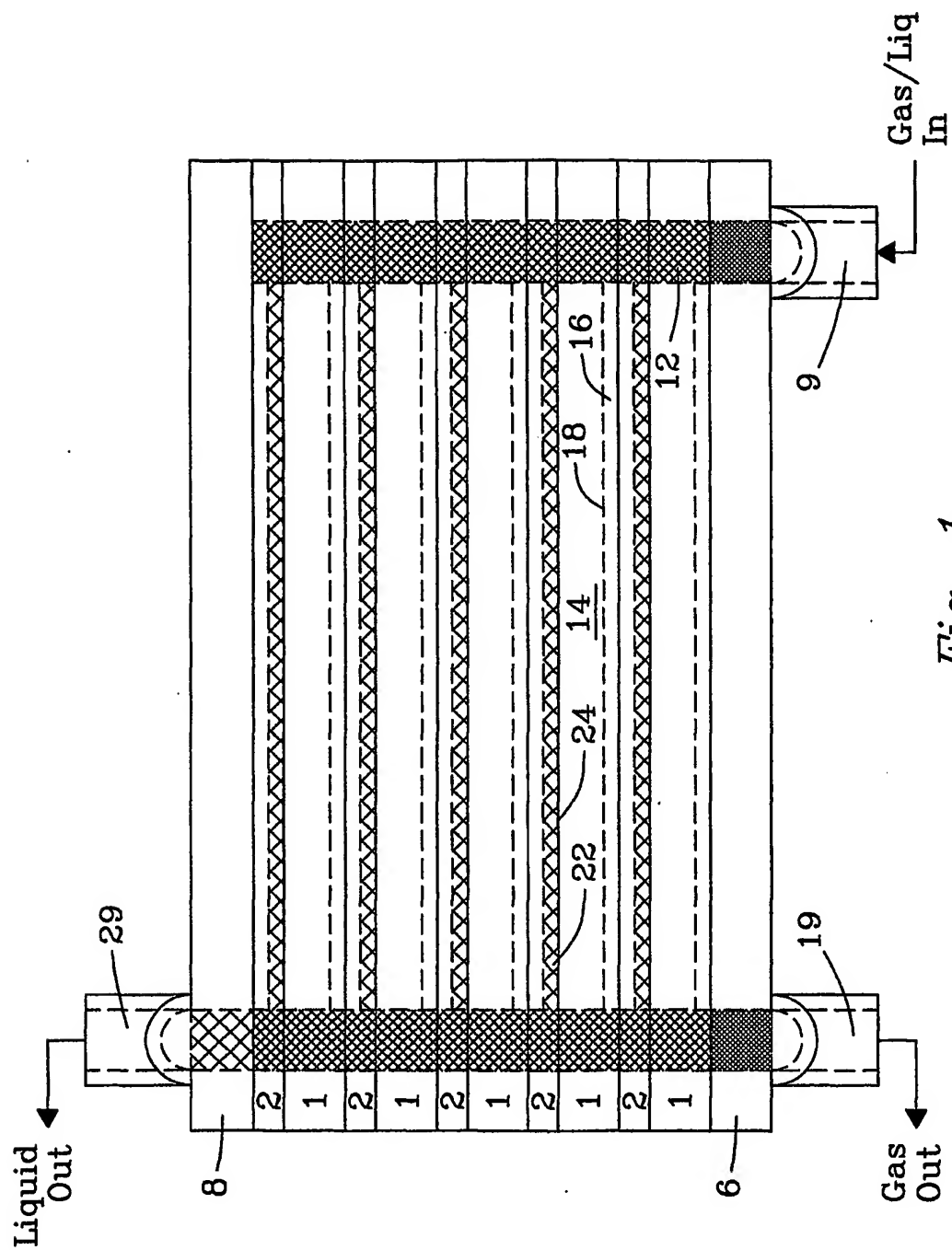
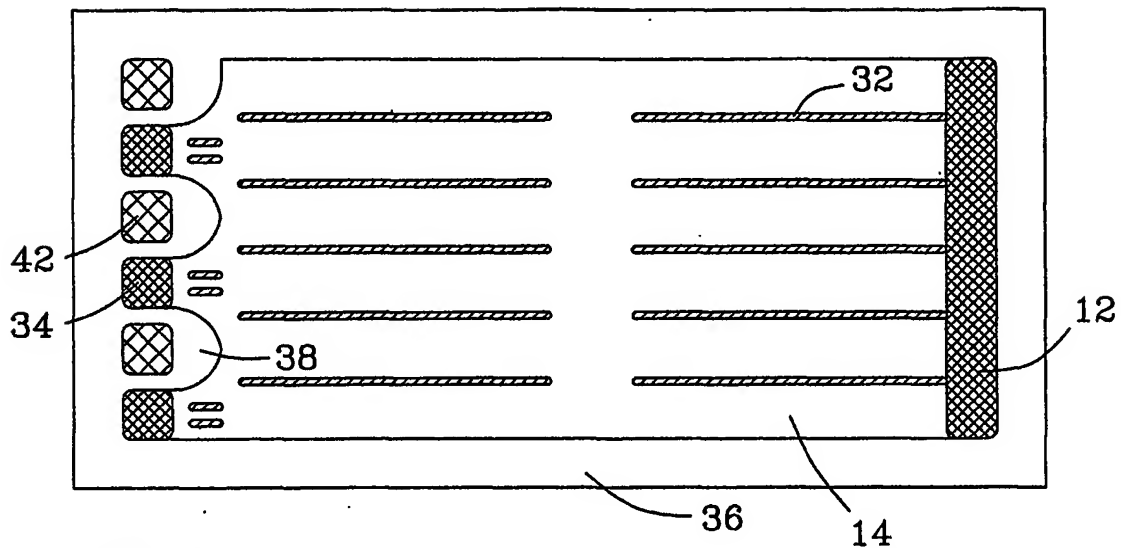


Fig. 1

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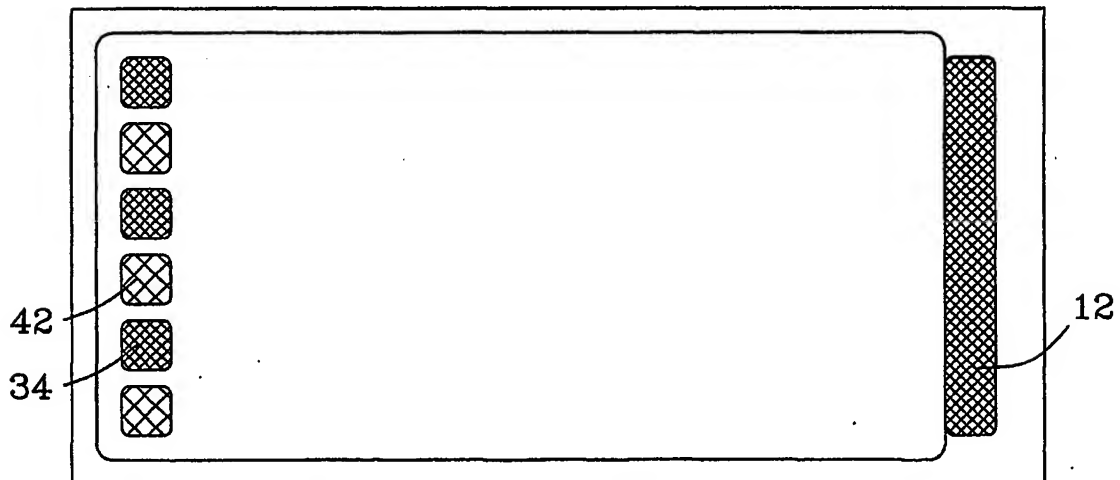
-  - Regions cut all the way through the shim
-  - Regions cut all the way through the containing wick structure
-  - Partially cut through the shim
-  - Lands in flow path (not cut)

Fig. 2*Fig. 3*

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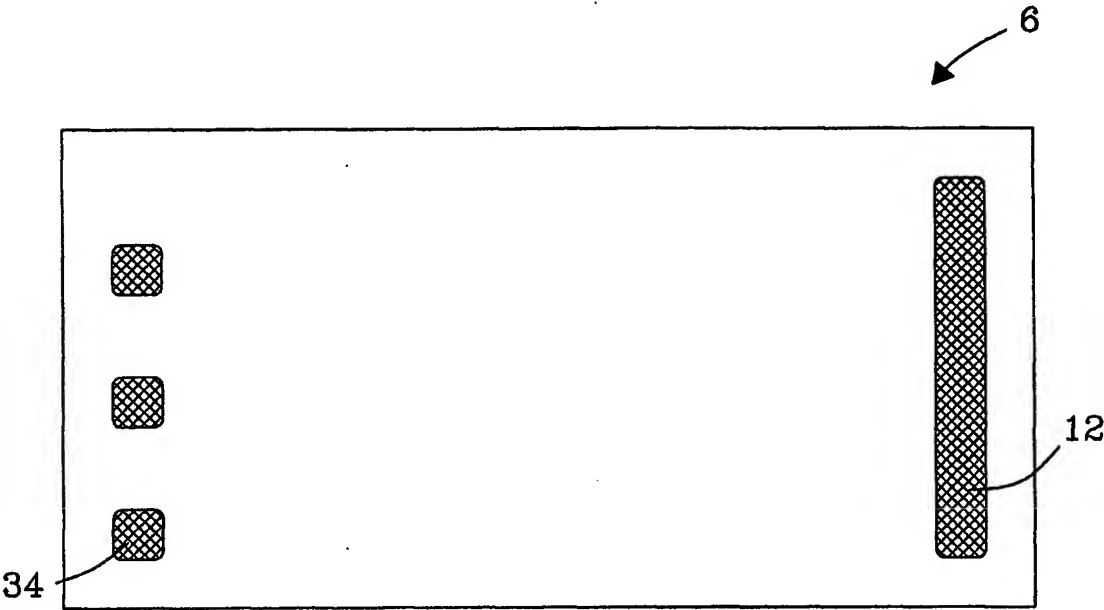


Fig. 4

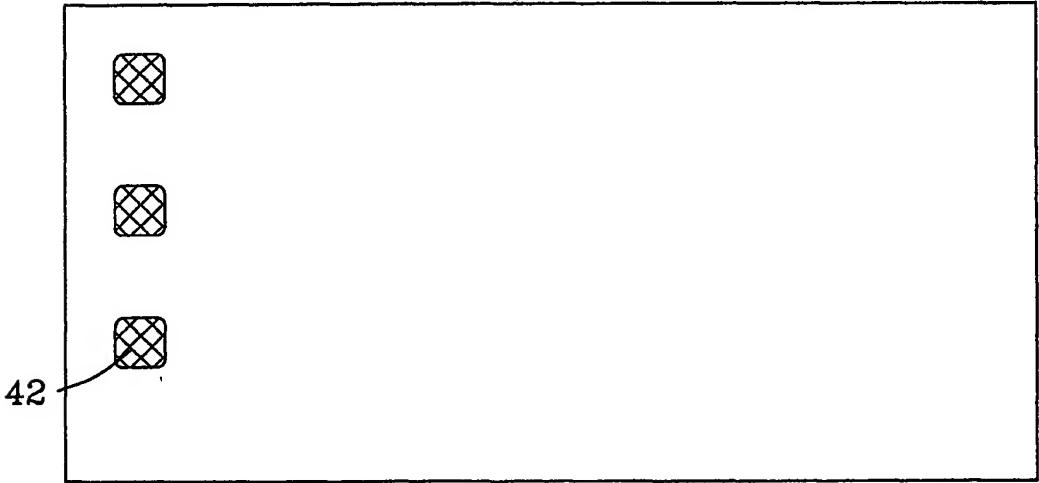


Fig. 5

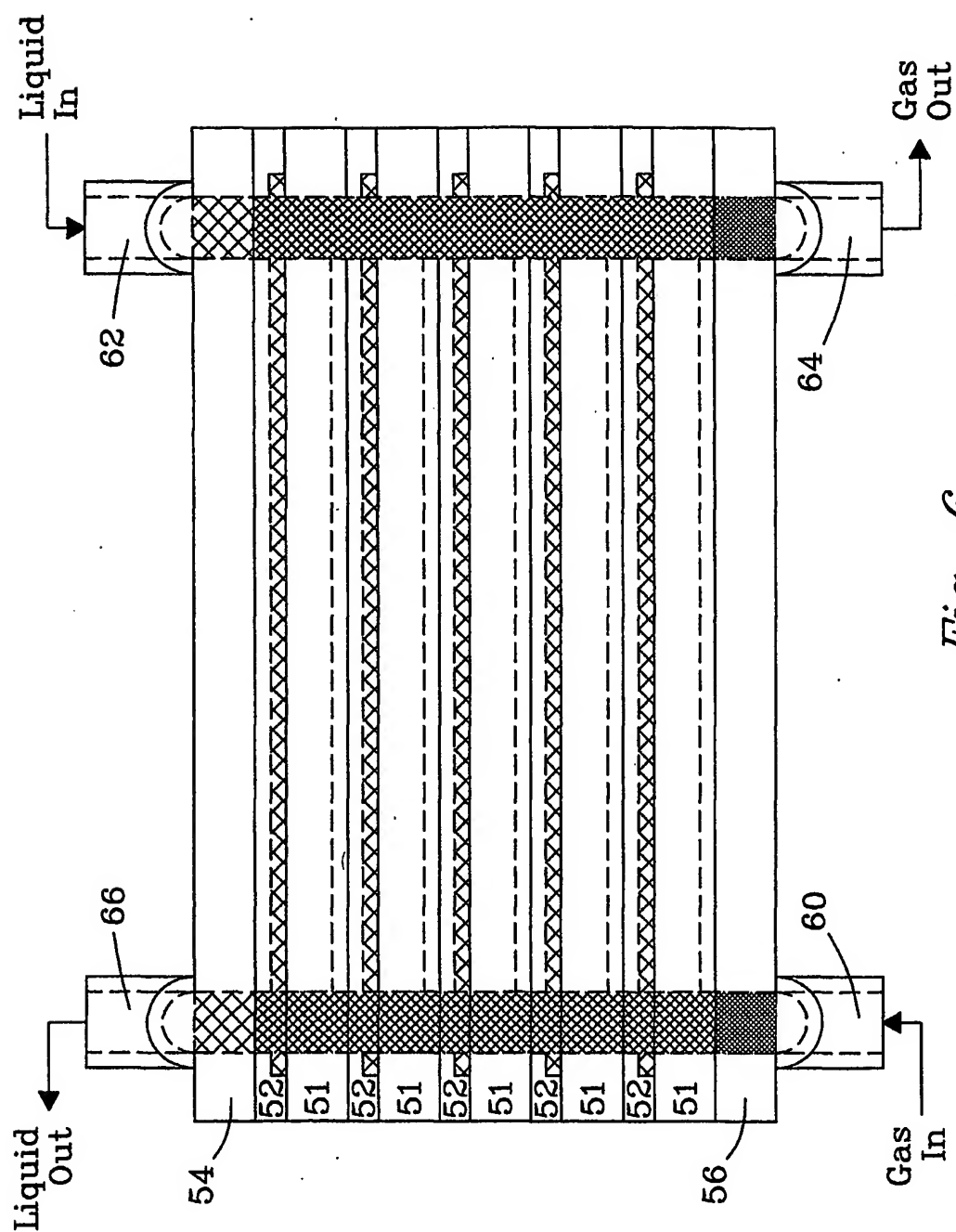


Fig. 6

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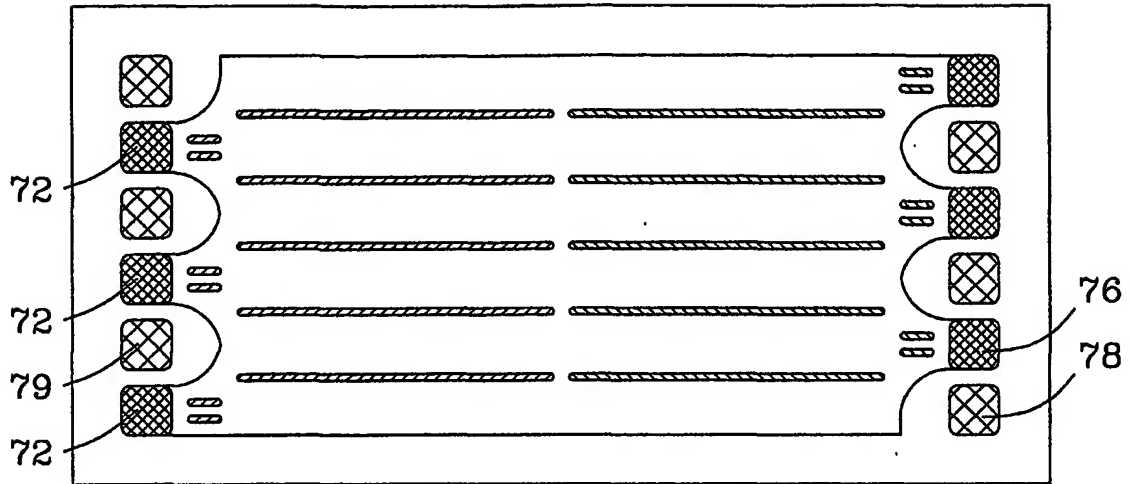


Fig. 7

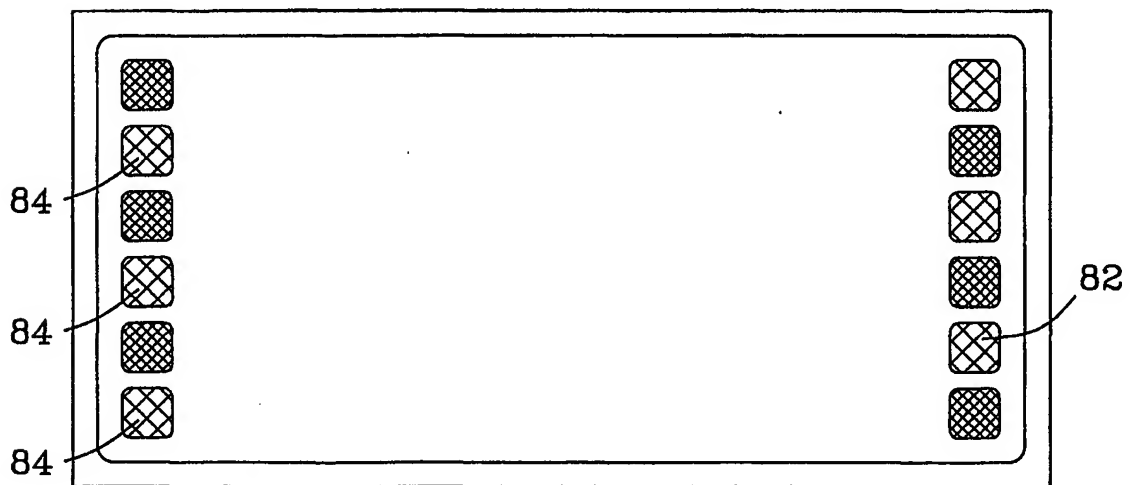
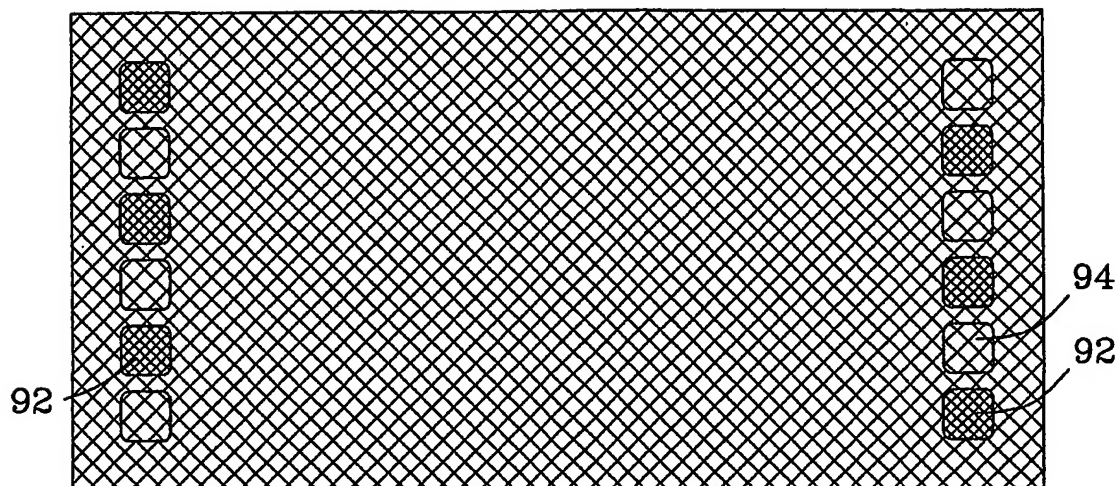


Fig. 8

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*Fig. 9*

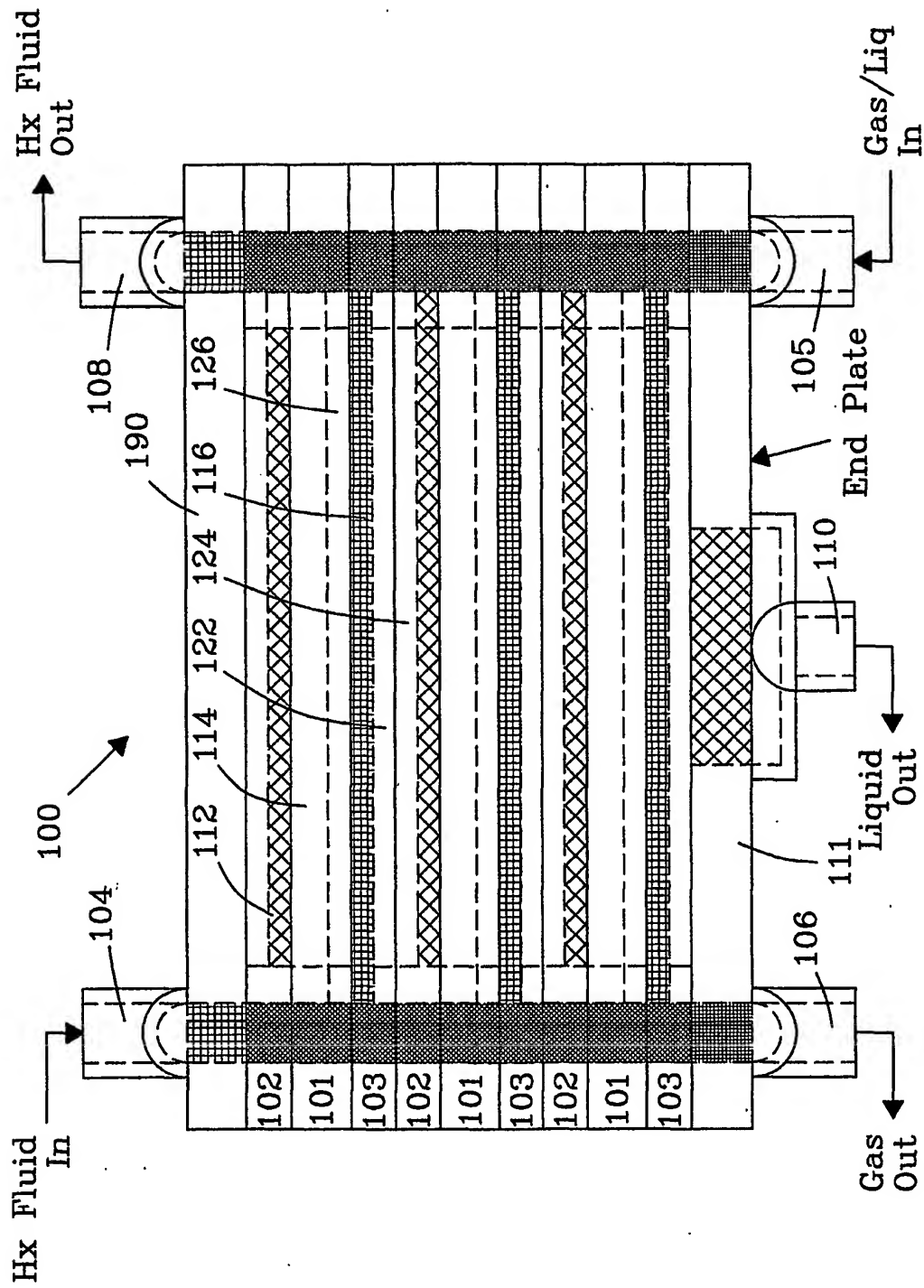


Fig. 10

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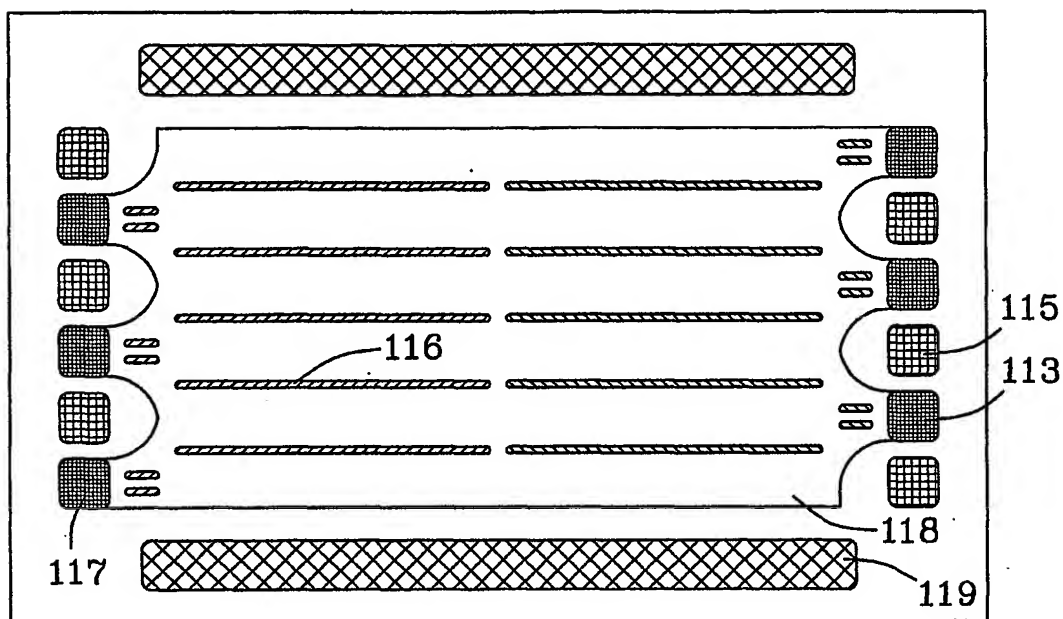


Fig. 11

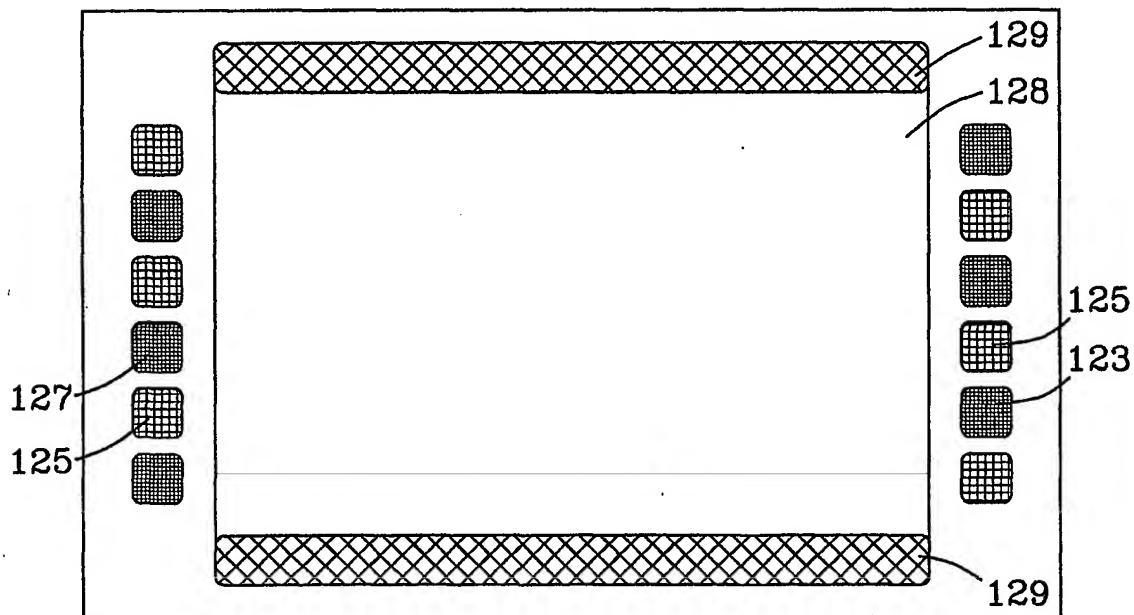


Fig. 12

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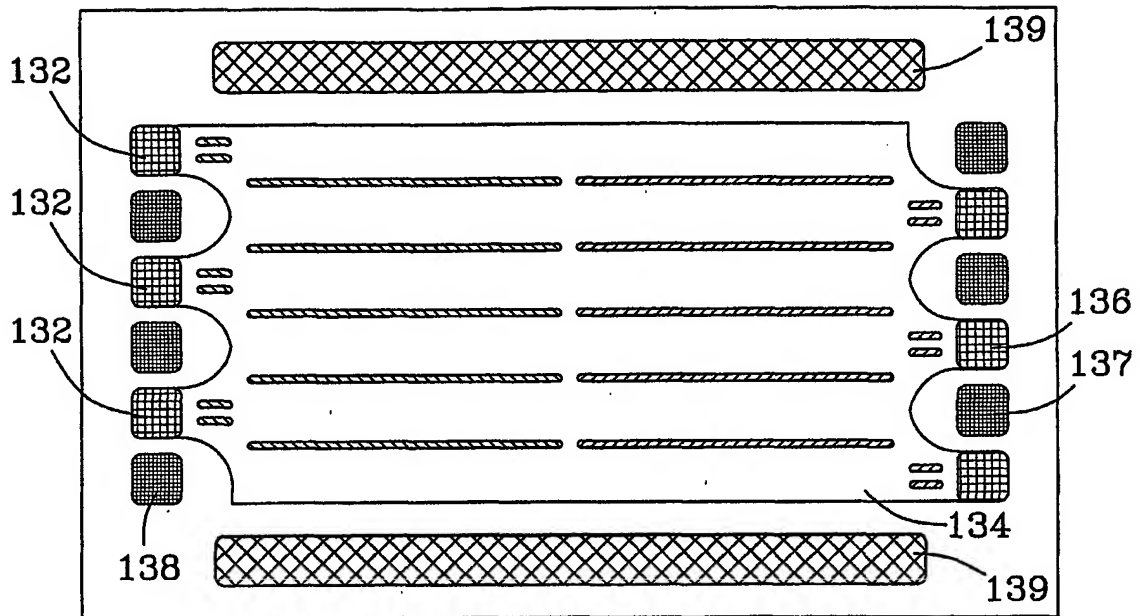


Fig. 13

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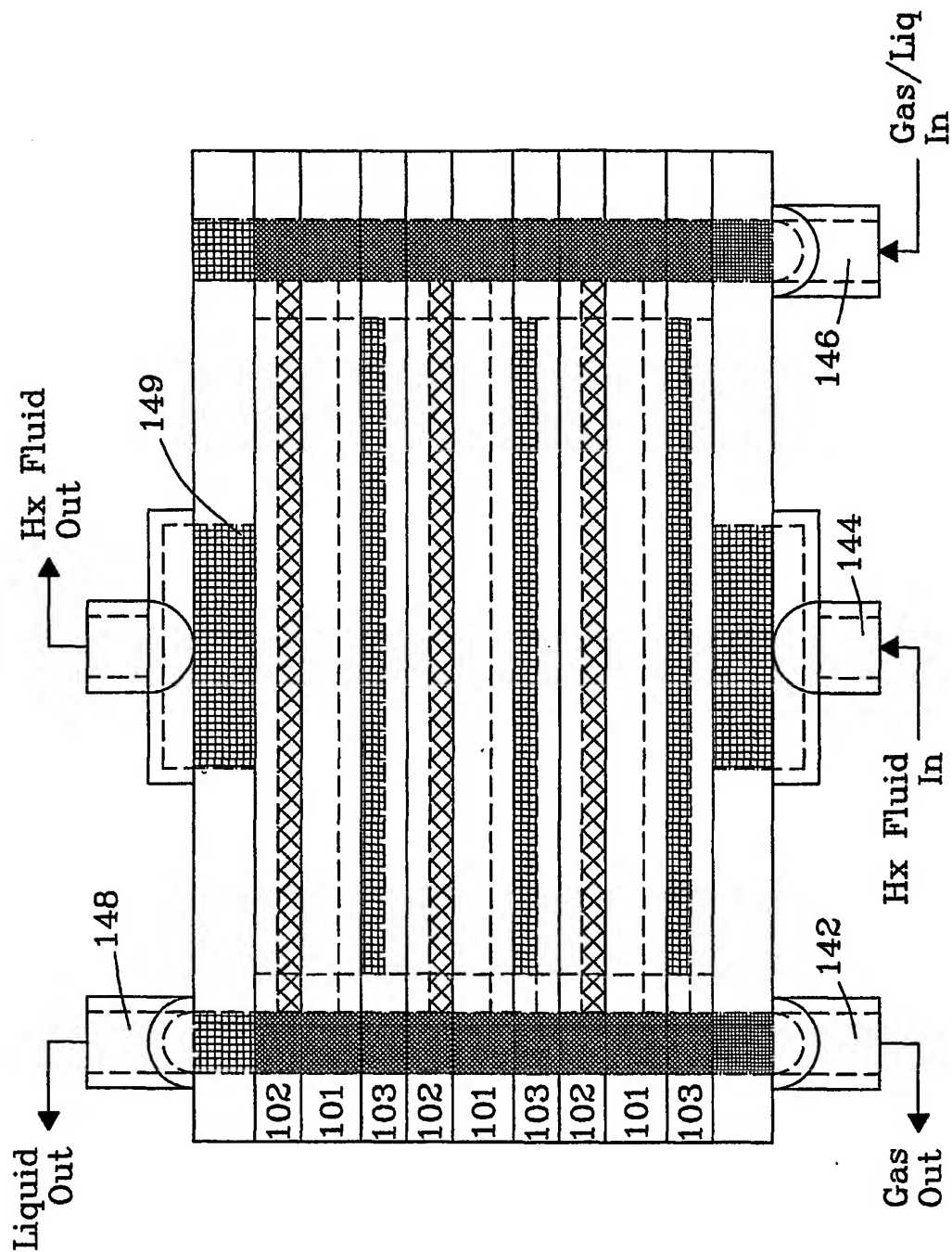


Fig. 14

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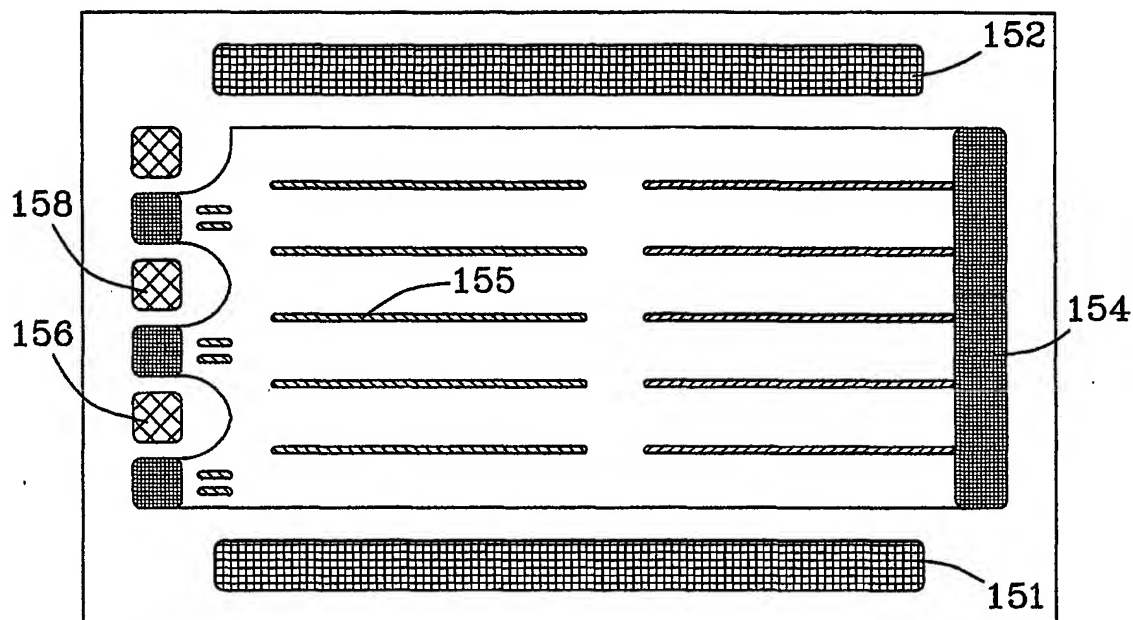


Fig. 15

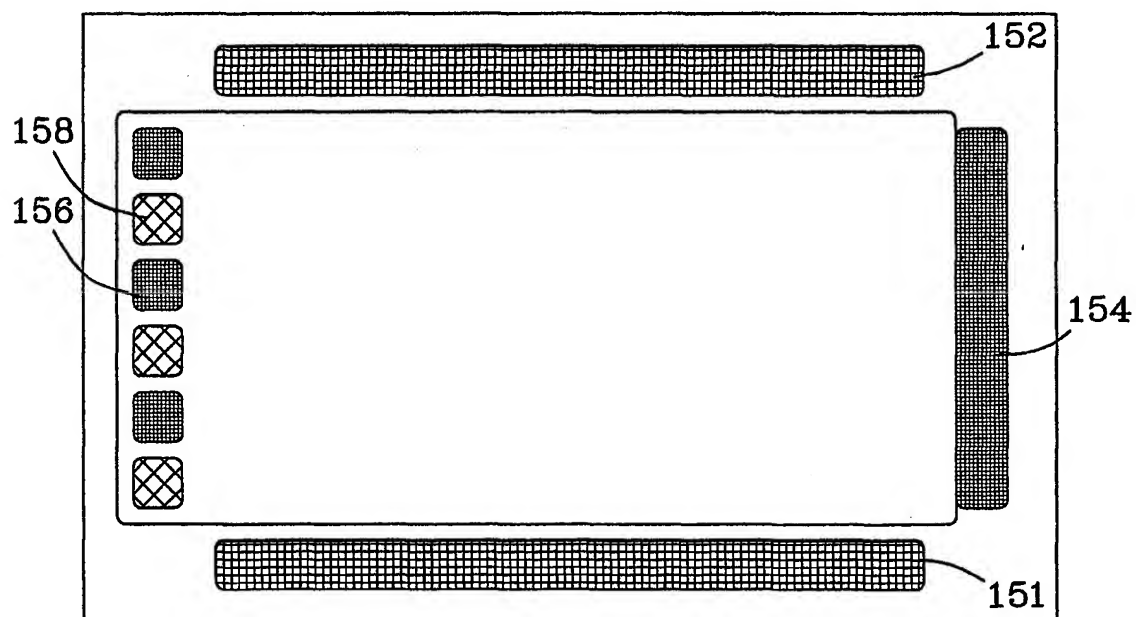
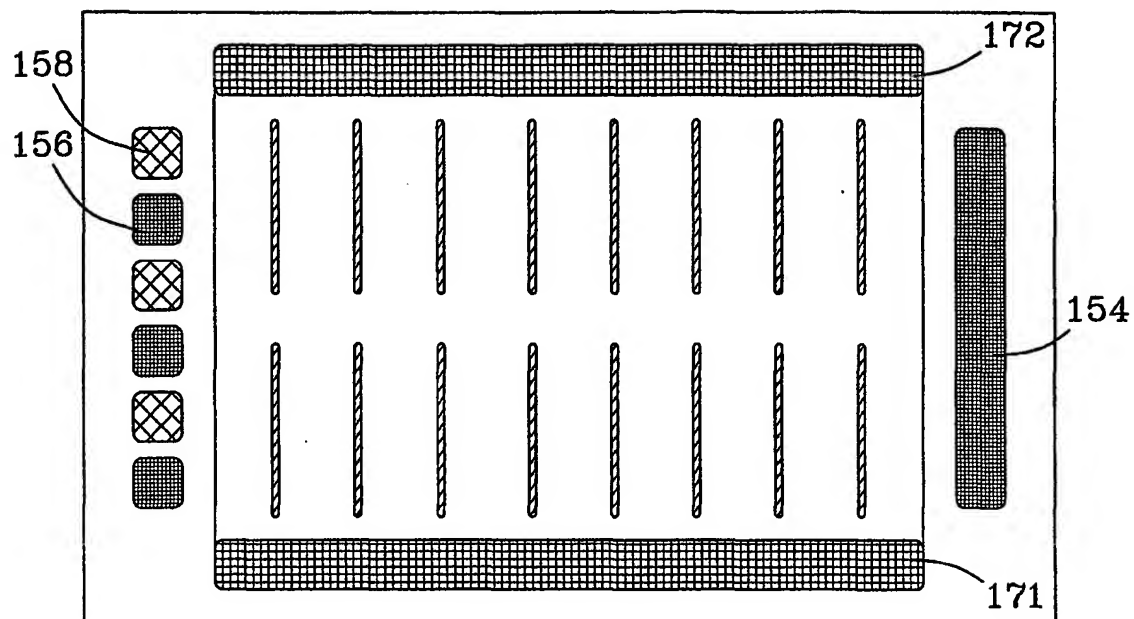
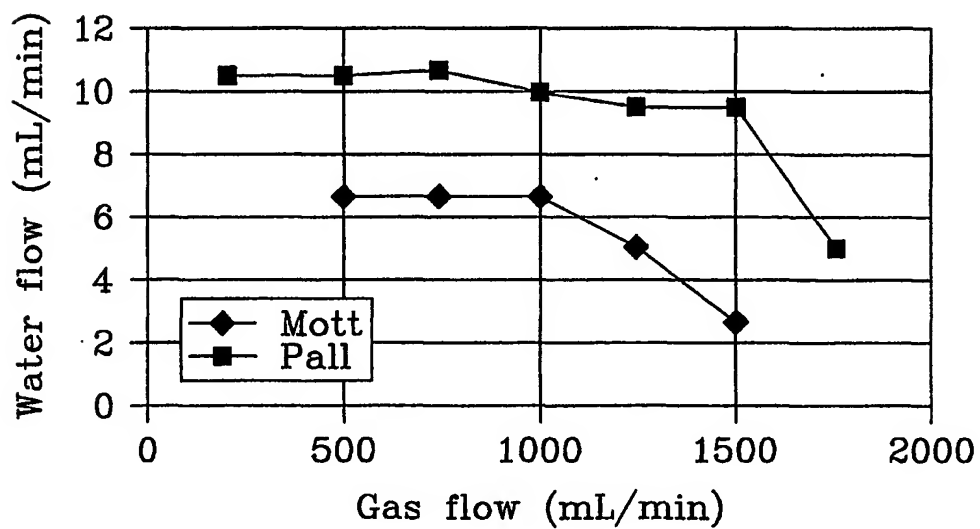


Fig. 16

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*Fig. 17**Fig. 18*